## EXPERIMENTAL CHECK ON A THEORETICAL MODEL FOR A CO<sub>2</sub> GDL BASED ON COMBUSTION PRODUCTS AT HIGH STAGNATION TEMPERATURES

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The working medium in a CO<sub>2</sub> GDL based on combustion products contains many components. The rapid advance in lasers of this type [1, 2] has been greatly facilitated by numerical calculations. A numerical model has been described [3-5] for a gasdynamic CO<sub>2</sub> laser based on the combustion products from C-H-O-N fuel, and a comparison has been made of the theoretical and measured weak-signal gains  $k_0$  for stagnation temperatures of  $T_0 = 1100-1800^{\circ}$ K/ the gain was chosen as the criterion because  $k_0$  is simple and easy to measure and is one of the basic parameters of the active medium. It was found that in this range in T<sub>0</sub> the model with the rate constants selected for it is suitable for quantitative description of the characteristics of a CO<sub>2</sub> GDL with a compound working medium over fairly wide ranges in the stagnation pressure  $p_0$ , medium composition, and flow expansion conditions.

The efficiency of a CO<sub>2</sub> GDL increases with T<sub>0</sub> at least up to 2500°K [1, 2, 6], and it is therefore necessary to perform calculations on the laser characteristics at high  $T_{0}$  over a wide range of compositions. The reliability of such calculations has to be examined. The equations for the vibrational energy-transfer kinetics given in [3] are applicalbe also at 1800-2500°K, since the lower vibrational levels of the molecules are mainly populated. However, many of the vibrational energy-transfer rate constants used in [3-5], in particular those for the rates of deactivation of the upper and lower laser levels of CO2, have been measured at 300-1000°K and extrapolated to higher temperatures. The variation of many of the rate constants at high To has little effect on the theoretical gain [4, 7] probably because the vibrational temperatures for the flow in the transonic region are initially close to the translational temperature, but then there is a rapid fall in the flow temperature, while the change in the stock of vibrational energy in the nitrogen is usually small within a short period (it is the less the narrower the neck and the larger the angle of the nozzle; such conditions are characteristic of profiled nozzles of minimal length with large degrees of flow expansion  $A/A_*$  as used at high T<sub>o</sub>). A population usually begins to arise at a translational temperature much less than  $T_o$ . To obtain the correct result it is necessary for the rate constants to provide equilibrium between the vibrational and translational degrees of freedom at high flow temperatures, and they have to have reasonably reliable values during the formulation of the population inversion. A final answer to this question can come from comparing theory with experiment, which is the purpose of the present study.

A detailed comparison has been made [7, 8] of numerical models for the vibrational kinetics analogous to that described in [3-5], and good agreement was obtained over the calculated and measured k<sub>0</sub> at high T<sub>0</sub>. However, in [7] the flow was that of a ternary mixture of CO<sub>2</sub>, N<sub>2</sub>, and H<sub>2</sub>O through a slot, while in [8] the mixture consisted of CO<sub>2</sub>, N<sub>2</sub>, H<sub>2</sub>O, and O<sub>2</sub> flowing brough a wedge nozzle with a relatively high throat and a small angle, i.e., under expansion conditions of little practical interest. This was responsible for the low gains found in [8]. Therefore, the results of [7, 8] do not allow one to draw conclusions on the reliability in calculations on CO<sub>2</sub> GDL using combustion products at high T<sub>0</sub>.

The literature shows that there have so far been virtually no measurements of  $k_0$  at  $T_0 > 1800$  °K with the expansion conditions for complex media required for this case; there is only [9], but in it the media consisted largely of  $CO_2$ ,  $N_2$ ,  $H_2O$ , and  $O_2$ , but the profiled nozzles had degrees of expansion insufficiently large for high  $T_0$ .

We have measured and calculated  $k_0$  for stagnation temperatures up to 2400°K for a series of multicomponent media covering almost all the limiting cases of working media for

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 $CO_2$  GDL based on combustion products, and we examined the flow through a profiled nozzle with a fairly large degree of expansion.

The experiments were performed with a GDL apparatus working in the quasistationary 1. state [4, 5, 10-12]. Combustion under isochore conditions was used with model fuel mixtures composed of C<sub>2</sub>H<sub>2</sub>, H<sub>2</sub>, CO, O<sub>2</sub>, N<sub>2</sub>O, CO<sub>2</sub>, N<sub>2</sub> [11] to obtain hot working media with given compositions and temperatures. The maximum temperatures  $T_{max}$  attained by burning these mixtures in a chamber were calculated from the measured maximum pressure. After the membrane separating the combustion chamber from the nozzle unit ruptured, the combustion products expanded through a planar profiled nozzle of minimum length (with a nodal point) having a height of the throat h =  $3 \cdot 10^{-4}$  m, A/A<sub>\*</sub> = 50, and a width of 0.4 m. The active media were probed at a distance of 0.053 m down the flow from the throat using a continuous-wave electric-discharge laser working on P18 transition in the  $00^{\circ}1-10^{\circ}0$  band of  $CO_2$ . In each experiment we recorded the dependence of  $k_o$  on  $p_o$  and  $T_o$ , which varied adiabatically as the medium flowed from the combustion chamber. This enabled us to find  $T_o$  from the known  $p_o$ . The heat transfer to the walls of the combustion chamber cannot be neglected at high To and was allowed for by increasing the effective adiabatic parameter by a factor  $1 + (S/S_*)St$  [13], where S and  $S_{\star}$  are the areas of the heat-transfer surface and the critical section of the nozzle, while St is the Stanton number. Figures 1 and 2 show measured ko (in Fig. 1, the crosses show  $k_0$  obtained in experiment 1, and the circles those in experiment 2, while the triangles relate to experiment 3; the crosses in Fig. 2 show ko obtained in experiment 4, and the triangles those in experiment 5). Table 1 gives the compositions of the model fuel mixtures (in mole %), the initial pressures  $p_i$  in the chamber before ignition, and the temperatures T<sub>c</sub> and T<sub>max</sub> obtained from thermodynamic calculations for the combustion of the mixture under isochore conditions. The stagnation parameters and the equilibrium compositions (in mole %) at the instants of measurement of  $k_0$  are given in Table 2. We see that the composition of the combustion products varied little in each experiment. The working media obtained in experiments 2-5 contained correspondingly more  $N_2$ ,  $H_2O$ , CO,  $O_2$  by comparison with the medium in experiment 1.

The overall error in measuring  $k_0$  was about 0.1 m<sup>-1</sup> at all levels. The error in measuring  $p_0$  was not more than 5%, but there was 10% error in determining  $T_0$ .

2. The calculation method has been described [3-5].+ The calculations were performed for  $T_o < 2500$  °K, so chemical processes in the flow were neglected [3, 5]. NO and OH occur +The V-T relaxation in the water vapor was incorporated in all the calculations.

TABLE 1

Experi- ment No.	C2H2	H,	co	O <sub>2</sub>	N20	CO2	$N_2$	p <sub>i</sub> ∙10 <sup>—5</sup> , Pa	т <sub>с</sub> , к	τ <sub>max</sub> , κ
1 2 3 4 5	5,0 2,2 3,4 2,9 3,9	 13,6 3,8 6,6	3,6 8,9 - 25,7 -	10,2 13,0 26,5	17,7 19,4		74,9 71,2 63,8 48,2 62,5	4,1 4,5 4,3 3,9 4,3	2500 2150 2500 2500 2500	2500 2100 2490 2350 2390

TABLE 2

Experi- ment No.	p₀·10 <sup>—5</sup> , Pa	<i>T</i> ₀, K	CO2	H₂O	N <sub>2</sub>	CO	02	NO	H₂	он
1	23,020,317,715,513,710,5 $8,06,2$	2400 2310 2220 2130 2045 1886 1734 1590	16,1 16,2 16,3 16,3 16,3 16,4 16,5 16,7	6,0 6,0 5,9 5,9 5,8 5,7 5,6	66,6 66,6 66,7 66,7 66,7 66,7 66,7 66,7	10,5 10,4 10,4 10,4 10,3 10,2 10,1 10,0			0,6 0,7 0,7 0,7 0,7 0,8 0,9 1,0 1,1	
2	22,3 16,5 12,2 8,8 6,3	2000 1800 1640 1480 1320	10,7 10,7 10,7 10,8 10,8	2,0 2,0 2,0 2,0 1,9	85,1 85,1 85,4 85,1 85,1 85,1	2,1 2,0 2,0 2,0 1,9			$\begin{array}{c} 0,1 \\ 0,1 \\ 0,1 \\ 0,2 \\ 0,2 \\ 0,2 \end{array}$	
3	25,3 20,3 15,2 10,1 7,1 5,1	2410 2260 2070 1820 1630 1470	10,0 10,1 10,2 10,4 10,6 10,8	$17,1 \\ 17,1 \\ 17,0 \\ 16,9 \\ 16,7 \\ 16,4$	$\begin{array}{c} 68,1\\ 68,2\\ 68,2\\ 68,2\\ 68,2\\ 68,2\\ 68,2\\ 68,2 \end{array}$	3,6 3,5 3,3 3,2 3,0 2,8			1,0 1,1 1,1 1,3 1,5 1,7	0,1 
4	25,3 20,3 15,2 10,1 7,1 5,1	2345 2197 2020 1796 1626 1468	8,3 8,4 8,6 8,8 9,1 9,4	4,4 4,3 4,2 3,9 3,7 3,4	63,8 63,8 63,8 63,8 63,8 63,8 63,8	21,421,421,221,020,720,4			2,0 2,1 2,2 2,4 2,7 3,0	
5	22,7 19,8 15,0 11,3 8,6 6,5 4,9	2300 2200 2024 1890 1700 1560 1430	8,7 8,8 8,8 8,8 8,8 8,8 8,8 8,8	10,8 10,9 10,9 11,0 11,0 11,0 11,0	65,3 65,4 65,6 65,7 65,8 65,9 65,9	0,1  	13,613,713,914,014,214,214,214;2	1,21,00,60,40,20,10,1		0,3 0,2 0,1 0,1 

in the combustion products at high  $T_{\boldsymbol{o}},$  so additional vibrational relaxation channels were considered:

 $CO(1) + NO(0) \rightarrow CO(0) + NO(1); \qquad (2.1)$ 

$$N_2(1) + NO(0) \rightarrow N_2(0) + NO(1);$$
 (2.2)

$$NO(1) + M \rightarrow NO(0) + M; \tag{2.3}$$

$$OH(1) + M \rightarrow OH(0) + M.$$
(2.4)

The calculations were based on measured [14] vibrational energy-transfer probabilities for channels (2.1) and (2.2):

$$p^{(2.1)} = \exp (1.7 \cdot 10^{-3}T - 9.7),$$
  
$$p^{(2.2)} = 10^{(3.8 \cdot 10^{-4}T - 4.14)},$$

Here T is temperature, °K. The probabilities of V—T relaxation were calculated from the Schwarz-Slavskii-Herzfeld theory [15]. The solid lines in Figs. 1 and 2 show the calculated gains. In all cases there is good agreement with experiment.



3. In [8] we find rate constants  $k^{(i)}$  different from those used above for vibrational relaxation channels important to a CO<sub>2</sub> GDL:

$$N_2(1) + H_2O \rightarrow N_2(0) + H_2O;$$
 (3.1)

$$CO_{2}(00^{0}1) + H_{2}O \rightarrow \begin{cases} CO_{2}(11^{1}0) + H_{2}O; \\ CO_{2}(03^{1}0) + H_{2}O; \end{cases}$$
(3.2)

$$CO_{2}(01^{1}0) + H_{2}O \rightarrow CO_{2}(00^{0}0) + H_{2}O.$$
 (3.3)

The value of  $k^{(3,1)}$  given in [8] is very low  $({}^{3}\cdot 10^{-17} \text{ cm}^3/\text{sec})$ , which appears to be due to a misprint;  $k^{(3,3)} = 1.449 \cdot 10^6/\text{T Pa}^{-1} \cdot \text{sec}^{-1}$  is too low at T > 600°K, while  $k^{(3,2)} = 2.898 \cdot 10^2 (1-\exp(-\theta/\text{T}))^3/[1-\exp(-\theta_3/\text{T}) \text{ Pa}^{-1} \cdot \text{sec}^{-1}$  is too low for T > 820 but too high for T < 800°K by comparison with the data of section 2 for the corresponding rate constants +  $(\theta_2 \text{ and } \theta_3 \text{ in the expression for } k^{(3,2)}$  are the characteristic vibrational temperatures for the deformation and asymmetric modes of CO<sub>2</sub>). Note that the values of  $k^{(3,3)}$  from [8] correspond to the calculations of [16].

The calculations were performed with the values of  $k^{(3,2)}$ ,  $k^{(3,3)}$  from [8]; instead of the rate constants for (3.1) used in Sec. 2, we used the following dependence of  $k^{(3,2)}$  on T:

$$k^{(3.1)} = \exp(4.29 - 28.78T^{-1/3}) / [1 - \exp(-\theta_4/T) \operatorname{Pa}^{-1} \cdot \operatorname{sec}^{-1}.$$
(3.4)

Here  $\theta_4$  is the characteristic vibrational temperature of the nitrogen. The dependence of  $k^{(3,1)}$  on T given by experimental studies [17-21] is close to that proposed in [21, 22].<sup>‡</sup> It gives lower values  $k^{(3,1)}$  at T  $\geq 1000^{\circ}$ K.

Initially, these rate constants are tested out on the results of experiments [24], which appear to be the most reliable. In these experiments, the dependence of  $k_0$  on  $H_2O$  concentration was measured at distances of 0.063 and 0.143 m from the throat. The calculations were performed by  $p_0 = 12.0 \cdot 10^5$  Pa,  $T_0 = 1540^\circ$ K for the flow of a ternary mixture with a molar proportion of nitrogen  $Y_{N_2} = 0.7$  through a profiled nozzle of minimum length with  $h = 2.3 \cdot 10^{-4}$  m and  $A/A_* = 30$ . The broken line in Fig. 3 shows the results for  $k_0$ , while the filled and open circles show the values of  $k_0$  found in [24] at distances of 0.143 and 0.063 m respectively. It is clear that at low  $H_2O$  concentrations  $(Y_{CO_2}/Y_{H_2O} > 15)$  the calculated values of  $k_0$  are much larger than the measured ones. The reason for this lies in the values of  $k^{(3,3)}$  at T < 800°K. For example, if we replace the T dependence of  $k^{(3,3)}$  from [8] by that used in Sec. 2 [4, 5], while leaving the values of the other rate constants unchanged, we obtain good agreement with experiment, as in [4, 5] (solid lines in Fig. 3).

Therefore, for the comparison with the experimental results described in section 1 we used the values of  $k^{(3,2)}$  from [8] in the calculations, with  $k^{(3,1)}$  given by (3.4), while the other rate constants, including  $k^{(3,2)}$ , were as in Sec. 2. The broken lines in Figs. 1 and 2 show the resulting values for  $k_0$ . The agreement with experiment is then worse than before, particularly at  $T_0 = 1700-2400$ °K.

<sup>+</sup>Curve 2 of Fig. 4 in [8] does not correspond to the data of [4] for the temperature dependence of  $k^{(3,3)}$ .

 $\ddagger$  In [22], a similar T dependence of  $k^{(3,1)}$  is shown in Fig. 4, but the analytic expression given, which was then used in [2], does not correspond to this but describes the results given in [23].

Therefore, the rate constants for vibrational energy transfer used in Sec. 2 are suitable also for  $T_0 = 1800-2400^{\circ}K$ , at least for the flow of a multicomponent working medium through a profiled nozzle with large  $A/A_{\star}$  and small h. These rate constants give a better description of the relaxation in the flow than those considered in Sec. 3.

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